

Electronic Supplementary Information (ESI) for RSC Advances.

Supporting Information

Preparation of Graphene Oxide Liquid Crystals with Long-range Ordered Flakes through the Coat-hanger die

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Lateral mean size of GO flakes

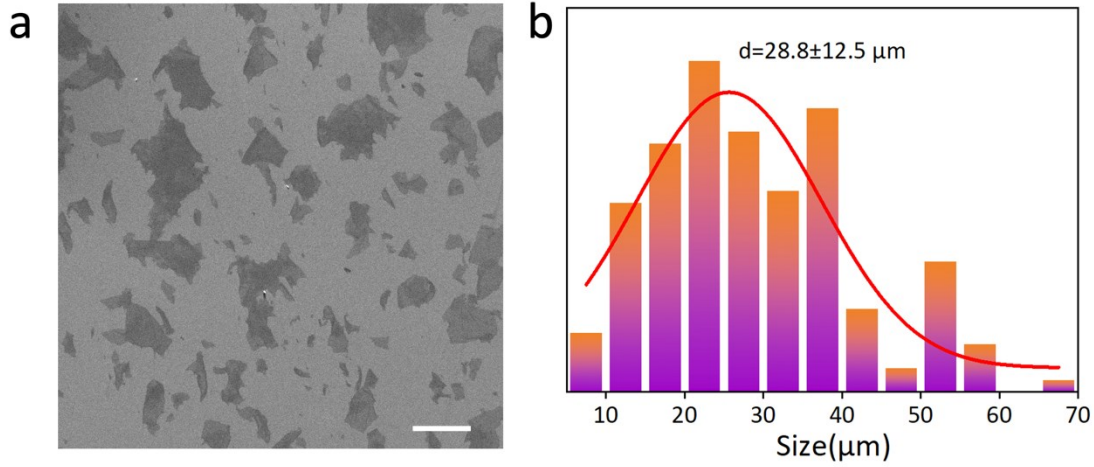


Fig. S1 (a) SEM of GO sheets of GO dispersions and (b) histogram of the sizes of GO sheets. The mean lateral size of GO flakes are around 30um.

Mathematical formulation of the coat-hanger die¹

The coat-hanger die in scheme 1 is shown here with following assumptions:

- 1) Polymer melt viscosity can be described by so called power-law equation (Eq 1).
- 2) Melt temperature is uniform throughout the flow stream.
- 3) The manifold is a circular tube and the coat-hanger has a constant gap.
- 4) Melt flow is laminar.
- 5) Melt in the coat-hanger section flows only along the machine direction.
- 6) Melt in the manifold flows only in the z-direction.
- 7) Residence time are the same in the die's manifold and slot.

According to the power law equation in Eq 1

The manifold radius $R(y)$ in y-axis direction expressed as follows:

$$R(y) = m^{\frac{1}{3(n+1)}} \cdot \pi^{-\frac{1}{3}} \cdot \left\{ \frac{(3n+1)}{2(2n+1)} \right\}^{\frac{n}{3(n+1)}} \cdot H^{\frac{2}{3}} \cdot (B-y)^{\frac{1}{3}} \quad (S1)$$

Where m is the ratio of residence time in the manifold to residence time in the slot; n is the flow behavior index in the Eq 1; H is the gap of the coat-hanger die section; B is the half of the coat-hanger width.

In our designed coat-hanger die, $m = 1$ according to the assumptions, H sets as 100 μm , B sets as 25 mm.

It is worth to mention that H is a control variable in our design. Theoretically, the shear rate is

inversely proportional to the gap size of the coat-hanger die according to Eq S2, which means that a smaller size of slot gap can better extrude the highly ordered GOLCs. The reason of H sets as 100 μm was that 100 μm was the minimum size that our 3D printer can stably print.

$$\dot{\gamma}_c = \pm \left(\frac{2n+1}{n} \right) \left(\frac{2Q_0}{BH^2} \right) \quad (S2)$$

Where Q_0 is the half of the total volumetric flow.

The height of manifold to the slot outlet of the

$$\begin{aligned} z(y) &= \int_0^z dz = \int_0^y \left\{ \frac{k'}{(B-y)^{\frac{2}{3}} - k'} \right\}^{\frac{1}{2}} dy \\ &= -\frac{3}{2} \cdot k^{\frac{1}{2}} \left[(B-y)^{\frac{1}{3}} \cdot \sqrt{(B-y)^{\frac{2}{3}} - k'} + k' \ln \left\{ (B-y)^{\frac{1}{3}} + \sqrt{(B-y)^{\frac{2}{3}} - k'} \right\} \right]_0^y \end{aligned} \quad (S3)$$

Where k' :

$$k' = m \frac{-2(3n+1)}{3(n+1)} (\pi H)^{\frac{2}{3}} \left\{ \frac{(3n+1)}{2(2n+1)} \right\}^{\frac{4n}{3(n+1)}}$$

The center height of the coat-hanger die, Z_c , is calculated as:

$$\begin{aligned} Z_c &= \int_0^{L-k^2} \left\{ \frac{k'}{(B-y)^{\frac{2}{3}} - k'} \right\}^{\frac{1}{2}} dy \\ &= -\frac{3}{2} \cdot k^{\frac{1}{2}} \left[k' \log_e \frac{B-k^2}{B} - B^{\frac{1}{3}} \sqrt{B^{\frac{2}{3}} - k'} - k' \ln \left\{ B^{\frac{1}{3}} + \sqrt{B^{\frac{2}{3}} - k'} \right\} \right] \end{aligned} \quad (S4)$$

Then, we calculated the dimensions of the coat-hanger die:

GO dispersions	n	K	B (mm)	H (μm)	R_0 (mm)	Z_c (mm)
GO-2	0.385	0.81	50	100	0.1553	3.9977
GO-4	0.260	3.80	50	100	0.1567	4.0777
GO-6	0.237	9.28	50	100	0.1570	4.0959
GO-8	0.235	14.14	50	100	0.1571	4.0976

GO-10	0.225	19.74	50	100	0.1572	4.1060
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Simulation results of shear rate and shear viscosity

The shear rate and shear viscosity of the flow at the die's outlet in x-axis. The extrusion pressure was set as a controlled variable here.

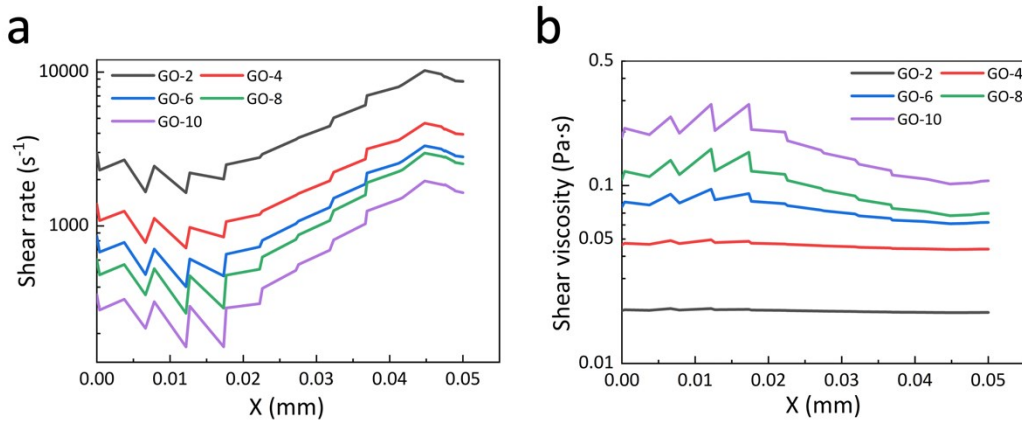


Fig. S2 Shear rate (a) and shear viscosity (b) of the simulation of the coat-hanger die in x-axis.

To investigate the changes in shear rate at different slot gap sizes, we designed three different coat-hanger die with 100 μm , 150 μm and 200 μm gap sizes according to the rheological properties of GO-10. The volumetric flow rate was set as a controlled variable in Fig. S3a to obtain the same velocity of the flow at the center of die's outlet. The shear rate in Fig. S3b was obtained from the differentiation of the flow velocities in Fig. S3a.

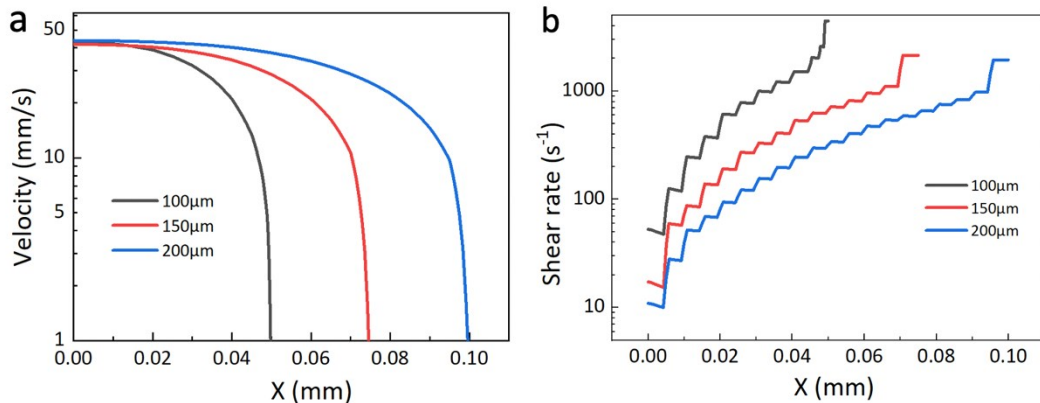
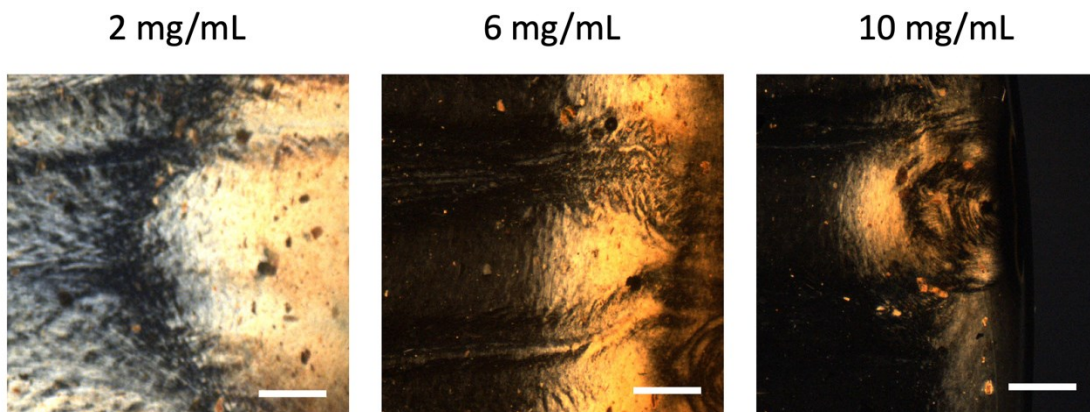


Fig. S3 a) The velocities of the flow at the outlet of the die in x-axis; b) The influence on shear rate of different slot gap sizes of the die; As mentioned that smaller gap sizes will increase shear rate in the die's slot.



Birefringent texture of GOLCs at the edge

Fig. S4 POM images of GOLCs at the edge of the extruded GO dispersions.

Raman spectra of GO and rGO foams

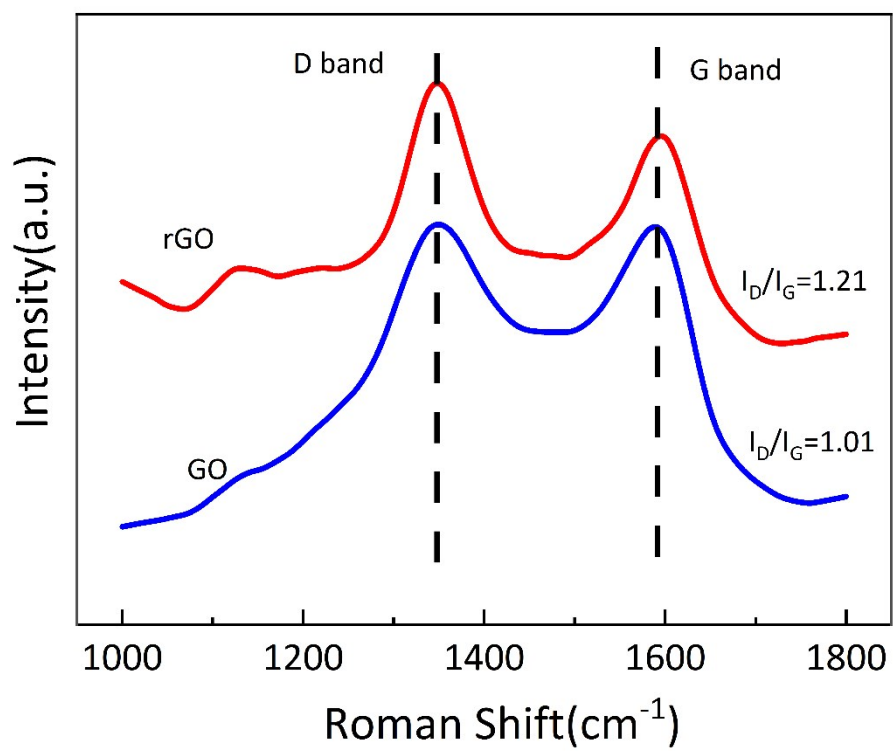


Fig. S5 Raman spectra of GO and rGO foams. I_D/I_G changes from 1.01 to 1.21 for GO and rGO respectively, indicating that the reduction process altered the structure of G-O.

1. Y. Matsubara, *Polym. Eng. Sci.*, 1980, **20**, 716–719.